Uwe D. Neue Award in Separation Science

- Uwe D. Neue: A Personal Reflection
- Thank You
 - Permanent Scientific Committee HPLC Conference Series
 - Sponsor of the Uwe D. Neue Award, Waters Inc. in particular Martin Gilar.
- Acknowledgements
 - Colleagues and Senior Management at Agilent Technologies world wide
 - My peers in academia
 - ••••





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Dipl.-Ing. FH Fred Strohmeier Colleague and peer. Now Senior Vice President, Life Sciences and Diagnostics Group



Current and Future Perspectives on UHPLC; Requirements for Improved Abilities and Functionality.

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Two key ingredients for this evolution

- Introduction of new ultra-high pressure stable sub-2-µmeter diameter particles followed by the introduction of superficially porous, low diameter particles in 2006
- Next generation HPLC instrumentation capable to deliver solvents at ultra-high pressure and able to conserve the ultra high efficiency separation of columns packed with these new particles



- Pioneered by Waters Inc. as UPLC[®] system with BEH particle technology (Uwe Neue as contributor) and Advanced Materials Technology with HALO particles (last year's Uwe Neue Award recipient Jack Kirkland).
- A plethora of UHPLC systems and column technology has followed since.

*An innovation is something original, new, and important in whatever field that <u>breaks into a market</u> or society. This is accomplished through <u>more effective products</u>, processes, services, technologies, or ideas that are readily available to markets, governments and society.

Source: http://en.wikipedia.org/wiki/Innovation

HETP and Pressure Drop vs. Solvent Velocity Dilemma





1 - Parameter Kinetic Optimization*



L (50 mm) and d_p fixed, select optimal u_o



*Slide courtesy of Prof. Ken Broeckhoven, Free University of Brussels

2- Parameter Kinetic Optimization (e.g. "Poppe Plot" approach)



Poppe's approach: find $u_{0,max}$ and $L(u_{0,max})$ corresponding to a given N_{req} and ΔP_{max} at a <u>fixed</u> particle size

The following relationship exists for "plate time":

$$\frac{t_0}{N} = \frac{H(u_0)}{u_0} \qquad \qquad \frac{H(u_0)}{u_0} = \frac{A \cdot d_p}{u_0} + \frac{B \cdot D_m}{u_0^2} + C \cdot \frac{d_p^2}{D_m}$$

In order to construct the plot of the plate time in dependence of N_{req} after obtaining the coefficients of the van Deemter equation (or e.g. the Knox equation) by non-linear regression, the Poppe plot can be calculated and substitution of the appropriate value for ΔP_{max} .

$$\log(t_0 / N_{req}) = \log C_1 N_{req}$$
 $C_1 = [h^2 \Phi_0 \eta / \Delta P^{max}]$ $h = H(u_0)/d_p$

So, when one wants to decrease the plate time and does not want to sacrifice separation time, the column resistance factor (Φ) should be reduced (e.g. monoliths!), viscosity decreased (η) (e.g. increase temperature!) or increase the max. available pressure

H Poppe, J. Chrom. A, 778, 3 (1997), G. Desmet et al., Anal. Chem., 77, 4058 (2005), F. Gritti and G. Guiochon, J. Chrom. A, 1228, 2, (2012)

2-Parameter Kinetic Plots for Different Particle Sizes





3-Parameter Kinetic Optimization (Knox & Saleem)



Find the maximum plate number possible when, u_o , L and d_p are varied to reach any ΔP_{max}

$$u_0^* = \left(\frac{\Delta P_{max} \cdot v_{opt}^2}{\Phi \cdot \eta}\right)^{0.25} \cdot t_0^{-0.25} \cdot D_m^{0.5} \qquad d_p^* = \left(\frac{\Phi \cdot \eta \cdot v_{opt}^2}{\Delta P_{max}}\right)^{0.25} t_0^{0.25} \cdot D_m^{0.5}$$

$$L^* = \left(\frac{\Delta P_{max} \cdot v_{opt}^2}{\Phi \cdot \eta}\right)^{0.25} t_0^{0.75} \cdot D_m^{0.5}$$

$$N_{\max}^* = \left(\frac{\Delta P_{\max} \cdot t_0}{\Phi \cdot \eta}\right)^{0.5} \cdot \frac{1}{h_{\min}}$$

Knox-Saleem limit

J.H. Knox and M. Saleem. J. Chromatogr. Sci., 7 (1969), p. 614 P. W. Carr, X. Wang, Anal. Chem. 2009, 81, 5342–5353

Maximum Achievable Plate Number vs. Pressure*





Preliminary Conclusions and Assumptions



Kinetic optimization predicts that the max. plate number achievable does not increase proportional with pressure

* More pressure will result in shorter time to obtain N_{reg} *

But

Such inferences from kinetic plots only apply if**:

- HETP is independent from column length
- physical and chemical properties of solvents and solutes, particle properties and column dimensions are independent of pressure
- frictional heating can be neglected

^{*}K. Broeckhoven and G. Desmet, accepted for publication in Trends in Analytical Chemistry

^{**}F. Gritti and G. Guiochon, J. Chrom., 1228, 2, (2012)



- Solvent properties
 - density (ρ), specific volume, viscosity (η), compressibility (χ) and melting point
- Solute properties
 - diffusion coefficient (D_m), molar volume, conformation/3D-structure changes (in particular with high MW substances)
- Retention factors (k) and in particular of ionizable molecules and HMW substances**
- Particle porosity and total porosity of the packed bed (ε_{T})
- Column dimensions length and diameter (L and d_c)

Under ultra-high pressure conditions, solute and solvent properties change but not independently!!

UHPLC – Constraints

Frictional Heating and Column Environment



$$Power = \triangle P \times F$$

Isothermal: fast heat exchange with constant temperature environment



Adiabatic: no heat exchange with environment





Unequal temperature distribution along the column axis

UHPLC – Constraints

Frictional Heating and Column Environment*





*experimental results courtesy of Monika Dittmann

which raises the bar

for following!!

UHPLC – Constraints

Extra Column Band-Broadening



$$\sigma_{v,col}^{2} = \sigma_{v,col}^{2} + \sigma_{v,inj.}^{2} + \sigma_{v,cell}^{2}$$

$$\sigma_{v,cap}^{2} = \frac{V_{cap}r^{2}u}{24D_{m}}$$

$$\sigma_{v,cell}^{2} = \frac{V_{cell}^{2}}{X}$$

$$redispersion factor, 1-12$$

$$\Delta P_{cap} = \frac{F \cdot 8\eta \cdot L_{cap}}{\pi r_{cap}^{4}}$$

$$\sigma_{v,column}^{2} = \frac{V_{0}^{2}}{N} \cdot (1 + k')$$
Detector



Mechanical & Hydraulic Engineering Challenges

- Switching and sealing interfaces, like piston-seal, check and rotary valves will become difficult to realize especially when the material strength limits are reached or materials more readily fatigues
- Pressure cycles will blow and relax the tubing in (sub)micrometer dimensions may damage bed structure and/or particles
- Narrower i.d. columns mandate lower flow rates and lower system volume and ultra-high pressure. Leaks will not noticeable, harder to find and eliminate. Significant influence on flow rate and composition precision and accuracy

UHPLC – Engineering Requirements

What is the force required to deliver solvents @ 1000 bar?

Desired flow rate 0.05 - 5 ml/min Piston diameter e.g. 3.1 mm, cross-section 7.6 mm² Stroke volume up to 100 μ l = 100 mm³ Desired flow rate precision (per channel) ~0.2%





UHPLC – Engineering Requirements

What is the force required to deliver solvents @ 1500 bar?

Desired flow rate 0.05 - 5 ml/min Piston diameter e.g. 3.1 mm, cross-section 7.6 mm² Stroke volume up to 100 μ l = 100 mm³ Desired flow rate precision (per channel) ~0.2%

Force ~ 1200N







- Constant Pressure Operation
- Multidimensional HPLC

UHPLC

Constant Pressure Operation





BENEFITS

- Super robust operation:
 - no overpressure shutdowns
 - "safety" pressure range necessary
- More efficient use of instrument power range, higher flow at lower viscosity
- Without pressure cycles, less stress on system and column
- 10-30% decrease of run time

UHPLC - Constant Pressure Operation

Signal Transformation



Measured run time axis into retention volume axis into equivalent "chromatographic" time axis. "Chromatographic" time = $\frac{Delivered Volume}{Hvpothetical Constant Flow}$



UHPLC - Constant Pressure Operation



Application Example



Elution order:

Thiourea, Atrazindesethyl, Hexanzinon, Metoxuron, Cyanazin, Methabenzthiazuron, Chlortoluron, Atrazin, Diuron, Metobromuron, Metazachlor, Nifedipin, Sebuthylazin, Terbuthylazin, Linuron, Prometryn, Nimodipin

Conditions and results:

Column: Eclipse plus C18, 1.8μ m, 2.1x100mm Constant Pressure: <u>1050bar</u>, 1.05 \rightarrow 1.4ml/min Constant Flow: <u>1ml/min</u>, 1020 \rightarrow 750bar

Time gain in Constant Pressure Mode: 10%

Further work, Desmet et al and Gritti & Guiochon

Multidimensional HPLC

Alternative?





* Slide courtesy of Dr. Stephan Buckenmaier, Agilent Technologies

Multidimensional HPLC 1D LC vs. 2D LC





Peak Capacity_{1D} =
$$150$$

$$Peaks_{1D} = 77$$

Peak Capacity_{2D} = 900 Peaks_{2D} = 174

Stoll, D. R.; Wang, X.; Carr, P. W. Anal. Chem. 2008, 80, 268–278.

Multidimensional HPLC

System Challenges





- User Interface for system control (including MS detectors)
- Quantitation and data representation

Multidimensional HPLC

Integrated systems and solutions are needed





<u>Tuesday, May 13, 5:15 pm-5:35 pm</u>

<u>L-149</u>: Improvements in Two-Dimensional HPLC Applications Enabled Advances in Instrument Technology.

by Stephan Buckenmaier et al., Agilent Technologies, Waldbronn, Germany

- 2x six loops instead of one gives 12 sampling positions
- High pressure selection valves for 2nd dimension UHPLC

* Slide courtesy of Dr. Stephan Buckenmaier, Agilent Technologies

Conclusions



- Raising the pressure bar does not increase N proportionally but N_{rea} is obtained faster
- At ultra-high pressure, physical, thermal and engineering constraints will make requirements for systems extremely challenging especially since columns have to be of lower i.d.
- Constant pressure operation is a viable option with operational benefits but has yet to be proven in practice
- Multidimensional LC will be a viable pathway for qualitative and quantitative analysis and high peak capacity but:
 - More dedicated and selective stationary phases for versatility and high orthogonality must be available.
 - Intelligent guidance of system set-up, valve control and automation that support the user.
 - Data handling, quantitation and representation will be demanding especially in combination with MS detection



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A PDF copy of this talk will be available on my website <u>http://www.rozing.com</u> after the talk (registration required)